Rheology of Gels Used for Conformance Control in Fractures

Jin Liu, SPE, and R.S. Seright, SPE, New Mexico Petroleum Recovery Research Center

Summary

This paper investigates whether gel behavior in rheometers correlates with that examined during extrusion through fractures. Although qualitative similarities were noted, the pressure gradients during gel extrusion through fractures were substantially greater than the values expected from rheological measurements. Also, the pressure gradient for gel extrusion through fractures varied in an unexpected manner with fracture width.

Introduction

Extensive investigations of extrusion of Cr(III)-acetate partially hydrolyzed polyacrylamide (HPAM) gels through fractures are described in Refs. 1 through 6. These experiments were both time-consuming and expensive. The question that we begin to address in this paper is this: Can the extrusion properties of gels in fractures be deduced from, or correlated with, results from simpler, less expensive rheological measurements?

Previous Rheological Work. Several earlier papers used rheological measurements to characterize gelants and gels used for conformance improvement in reservoirs. $^{7-14}$ As part of their work, these studies employed dynamic viscometry measurements to monitor gelation. However, they also studied gel properties after gelation. Prud'homme *et al.* 7,8 emphasized that small-amplitude oscillatory measurements could be used to study gels while causing minimum disruption to the gel structure. For a Cr(III)-HPAM gel, they found the elastic modulus, G', was independent of the frequency of deformation over the range 0.0016 to 16 Hz. They also noted that G' was directly proportional to the density of crosslinks in a gel. $^{7-9}$

Aslam *et al.*¹⁰ reported that Cr(III)-HPAM gels behaved as Bingham plastics under steady shear, exhibiting a linear relation between shear stress and shear rate above a yield stress. However, they examined a fairly small range of shear rates (4 to 75 s⁻¹). They also noted that gels were susceptible to shear degradation during steady shear experiments. Gels that formed at low shear rates gave higher apparent viscosities than those formed at high shear rates.

Thurston *et al.*¹¹ studied both HPAM and xanthan polymers that were crosslinked by Cr(III). After gelation, they noted that the elastic component of viscosity for mature gels was much greater (~100 times) than the viscous component. Consistent with the findings of Prud'homme *et al.*,⁷ Thurston *et al*¹¹ found that the elastic component of stress was independent of frequency from 0.3 to 30 Hz. Furthermore, the elastic component of stress for a 0.6% HPAM gel was seven times greater than that for a 0.3% HPAM gel. No significant shear degradation was evident during their oscillatory measurements.¹¹

Kakadjian *et al.*¹² studied two Cr(III)-acetate-HPAM gels and one HPAM polymer that were crosslinked with an organic crosslinker. They proposed that *G'* measurements should be used in place of bottle "tonguing" tests as a more quantitative measure of gel strength. Consistent with earlier studies, they also found that *G'* was nearly constant for frequencies from 0.1 to 10 Hz. For 3-day-old Cr(III)-acetate-HPAM gels at 40°C, they studied how sodium acetate content affected *G'*. As sodium acetate concentrations increased from 0 to 0.2 molar, *G'* decreased by 15 to 20%.

Copyright © 2001 Society of Petroleum Engineers

This paper (SPE 70810) was revised for publication from paper SPE 59318, first presented at the 2000 SPE/DOE Improved Oil Recovery Symposium, Tulsa, Oklahoma, 3–5 April. Original manuscript received for review 20 November 2000. Revised manuscript received 5 December 2000. Manuscript peer approved 21 December 2000.

Allain and Salome¹³ studied gelation of HPAM by Cr(III) using rheological and spectroscopic methods. They related measurements of viscosity and elastic modulus to the number of crosslinks formed during gelation. They suggested that at the gelation threshold, the average number of crosslinks per polymer chain was approximately 10. In contrast, classical theory predicted that the average should be one crosslink per chain. The discrepancy was attributed to intramolecular ("intrablob") crosslinks.

Recently, Broseta *et al.*¹⁴ used rheological measurements to study Cr(III)-acetate-HPAM gelation as a function of temperature, crosslinker concentration, polymer concentration, and polymer molecular weight. They also applied a force balance to develop an equation that they speculated might relate gel yield-stress to the maximum pressure drawdown that a gel could withstand in porous rock.

Basic Rheological Concepts

Cr(III)-acetate-HPAM gels are viscoelastic, meaning that their properties are intermediate between those of elastic solids and viscous liquids. For an elastic solid, application of a shear stress, τ_s , causes the solid to deform by a "strain" or distance, γ . If the stress is not too large, the solid relaxes to its original shape after the stress is removed. If the solid follows Hooke's law, the relationship between applied stress and strain is linear. ¹⁵ The ratio of stress to strain is called the shear modulus, G.

If the solid is deformed too much, the deformation may become plastic, meaning that the solid does not completely relax to its original shape after the stress is released. For common solids, the point (stress) at which plastic behavior begins is labeled the yield point (or yield stress).

For viscous fluids, no elastic deformation occurs when a shear stress is applied. Instead, the fluid flows, dispersing the applied force and energy as heat. ¹⁶ Viscosity, μ , is defined as shear stress divided by shear rate, $\dot{\gamma}$.

$$\mu_{w} = \tau_{s}/\dot{\gamma}$$
.(1)

For Newtonian fluids, viscosity is independent of shear rate.

For a viscoelastic material, elements of both elastic and viscous character are exhibited. ¹⁶ Depending on the time scale over which the stress is applied, either the elastic or the viscous nature may dominate performance. Usually, the elastic nature dominates over short time scales, while the viscous nature becomes more evident over longer time scales.

A common method to assess the viscoelastic nature of materials uses measurement of stresses during application of a sinusoidally oscillating shear strain. The applied strain, γ , is described with Eq. 2.

$$\gamma = \gamma_o \sin(\omega t). \qquad (2)$$

Here, γ_o =the maximum strain applied and ω =the angular frequency of the strain wave. The top curve in **Fig. 1** illustrates this strain wave.¹⁶

In a plate-plate viscometer, movement of one plate and deformation of the material between the plates generates a stress wave, τ , that is measured at the second plate.

If the material is an elastic solid, then the phase angle, δ , in Eq. 3 is zero. In contrast, if the material is a normal liquid, the phase angle is 90°. If the tested material is viscoelastic, the stress wave will be shifted by an intermediate phase angle, as illustrated by the

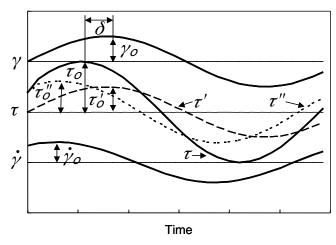


Fig. 1—Illustration of dynamic measurements.

middle solid curve of Fig. 1. For analysis, the stress wave is generally separated into two waves with the same frequency (dashed curves in Fig. 1). One wave (τ' in Fig. 1) is in phase with the strain wave, while the other wave (τ'' in Fig. 1) is 90° out of phase with the strain wave. In this way, the stress wave is separated into an elastic component and a viscous component.

Using the terms illustrated in Fig. 1, the elastic modulus or storage modulus, G', is defined by Eq. 4.

$$G' = \tau_o'/\gamma_o$$
.(4)

Similarly, the viscous modulus or loss modulus, G'', is defined by Eq. 5.

$$G'' = \tau_o''/\gamma_o$$
. (5)

The phase angle or loss angle, δ , is related to G' and G'' through Eq. 6.

$$\tan \delta = G''/G'. \qquad (6)$$

The bottom curve in Fig. 1 shows shear rate vs. time. Shear rate, $\dot{\gamma}$, is defined by Eq. 7.

$$\dot{\gamma} = \mathrm{d}\gamma/\mathrm{d}t$$
. (7)

As indicated in Fig. 1, the τ' wave is in phase with the strain (γ) wave, while the τ'' wave is in phase with shear rate $(\dot{\gamma})$.

The complex viscosity, $|\mu^*|$, is defined by Eq. 8.

The complex modulus, $|G^*|$ is defined by Eq. 9.

$$|G^*| = [(G'')^2 + (G')^2]^{0.5} = \tau_o/\gamma_o = |\mu^*|\omega.$$
 (9)

In this paper, we consider whether rheological measurements can be related to the behavior observed during gel extrusion through fractures. At first glance, an analogy is expected between gel extrusion through fractures and deformation between two plates in a rheometer. During extrusion through fractures, gel propagation may occur by a continual sequence of gel stretching, failure of either gel-gel bonds or gel-wall bonds, and finally, temporary relaxation of stretched gel blobs. Therefore, we examine whether results from extrusion experiments in fractures correlate with either oscillatory or steady shear rheological measurements.

Elastic and Viscous Moduli vs. Strain

When a gel is extruded through a fracture, several important questions arise.

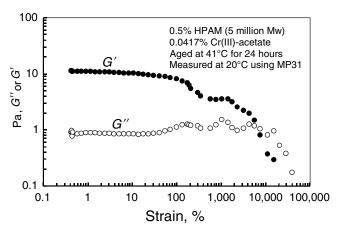


Fig. 2—Elastic (G') and viscous (G'') moduli vs. strain.

- 1. How far can the gel be stretched or deformed before it breaks?
- 2. Does the gel's elastic character dominate over its viscous nature?
- 3. How do the gel's properties vary with composition, temperature, and deformation rate?

We begin to answer these questions in **Fig. 2**, which plots the elastic (G') and viscous (G'') moduli vs. strain for a 24-hour-old Cr(III)-acetate-HPAM gel that contained 0.5% Ciba Alcoflood 935 HPAM (molecular weight $\sim 5 \times 10^6$ daltons; degree of hydrolysis 5 to 10%), 0.0417% Cr(III) acetate, 1% NaCl, and 0.1% CaCl₂ at pH=6. The formulation was prepared at room temperature and aged for 24 hours at 41°C. Subsequently, rheological measurements were performed at 20°C using a Paar-Physica UDS 200 Universal Dynamic Spectrometer with an MP31 (50-mm diameter) plate and 1 Hz oscillation frequency.

The solid circles show G'. At low strain values, the elastic modulus was near 10 Pa. As strain increased to 200%, G' gradually decreased to 6 Pa. However, the elastic modulus was reasonably constant over this range. Thus, the gel showed near-Hookean behavior over a significant range of stretching.

For strains between 200 and 4,300%, G' decreased from 6 to 2 Pa. Although the elastic component was not linear over this range, the result emphasizes this gel's tremendous ability to stretch—up to 4,300%! Thus, the utility of this gel during extrusion through fractures is not surprising.

For strains above 4,300%, G' rapidly decreased, indicating irreversible gel breakage.

The open circles in Fig. 2 show the viscous modulus (G'') vs. strain for the Cr(III)-acetate-HPAM gel. Over most of the range of strain values, G'' was about 1 Pa. Especially for the lower strain values, G'' was about one-tenth G'. Thus, the elastic nature of the gel dominated over its viscous nature.

Yield Stress

During gel extrusion through fractures, we noted that a minimum pressure gradient must be applied for the gel to flow.^{2–4} This observation suggests that the gel has a characteristic yield stress. Can the yield behavior noted during extrusion through fractures be correlated with stress measurements in a viscometer?

Fig. 3 plots shear stress vs. strain for the Cr(III)-acetate-HPAM gel that was aged for 24 hours at 41°C. As strain increased from 0 to 200%, stress increased linearly. However, as strain increased further, the stress-strain relation changed significantly. The lines drawn to fit the data in Fig. 3 show two attempts to define a yield stress for this gel. The intersection of the first two lines suggests that the yield stress was about 10 Pa, and that the strain value at the yield point was about 200%. However, other choices could be made. For example, the intersection of the upper two lines suggests a yield stress of 51 Pa that occurred at a strain of 1,400%. A third choice might be the greatest stress observed during the stretching process, which happened to be 88 Pa at a strain of 4,300%. For higher strains, the stress decreased, presumably because of irreversible breakage of the gel. Thus, uncertainty exists about the choice of a yield point.

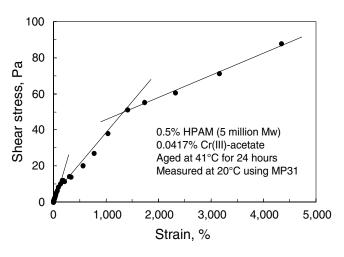


Fig. 3—Yield-stress determination.

Earlier, the pressure gradient required for gel extrusion was shown to be inversely proportional to the square of fracture width (**Fig. 4**, from Ref. 4). Was this behavior expected? For a material with a yield stress, τ_y , a simple force balance¹⁴ predicts that the pressure gradient required for extrusion should be given by Eq. 10.

$$dp/dL = 2\tau_y/w_o.$$
 (10)

In this equation, w_0 was the effective opening size during extrusion. The $1/w_0$ dependence from Eq. 10 apparently contradicts the $1/(w_f)^2$ dependence shown in Fig. 4.

For our standard 1-day-old Cr(III)-acetate-HPAM gel, our discussion of Fig. 3 suggested three possible choices for the yield stress—10, 51, or 88 Pa. Using these values and an opening size of 0.1 cm (0.04 in.), Eq. 10 predicts pressure gradients of 20, 102, and 176 kPa/m. In contrast, the experimentally measured values ranged from 633 to 1,130 kPa/m when the fracture width was 0.1 cm. Therefore, all yield-stress choices from Fig. 3 led to an underestimation of the pressure gradient during extrusion through a fracture. Thus, additional work must be performed to understand the relation between stress, fracture width, and the pressure gradient for gel extrusion.

Stress and Viscosity vs. Shear Rate

Another important issue when measuring stress is the rate at which the strain or deformation was applied. For our 24-hour-old Cr(III)-acetate-HPAM gel, **Fig. 5** plots shear stress and complex viscosity (defined by Eq. 8) vs. shear rate. The slope of the viscosity-vs.-shear-rate curve was approximately -0.8. This value compares with slopes between -0.83 and -0.95 for resistance-factor-vs.-velocity curves during gel extrusion through tubes and fractures.³

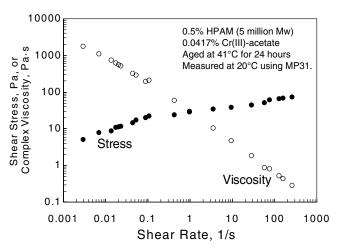


Fig. 5—Stress and complex viscosity vs. shear rate.

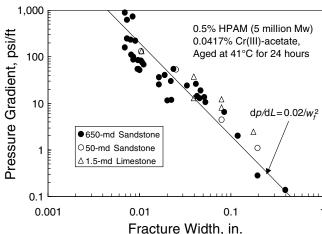


Fig. 4—Pressure gradients during extrusion.

Note in Fig. 5 that shear stress was fairly insensitive to shear rate. When shear rate increased by a factor of 100,000, shear stress only increased by a factor of 10. This result was consistent with our earlier observations that the pressure gradient required to extrude a gel through a fracture was fairly insensitive to injection velocity.¹⁻⁴

These similarities between behavior in fractures and in a viscometer provide hope that a useful correlation can be found.

Strain vs. Time

As mentioned earlier, the time scale for a deformation affects whether a material's elastic nature dominates over its viscous nature. For the experiments described in Fig. 2, the time scale for the deformation was 1 second (because 1-Hz oscillation was used). If a fixed stress is applied to a sample, how rapidly will the gel's strain response occur? For the Cr(III)-acetate-HPAM gel, this question is answered in **Fig. 6.** Various stress values (ranging from 2 to 20 Pa) were applied rapidly to the gel sample, and the strain was noted vs. time. For stresses of 10 Pa and below, the strain response appeared complete within 1 second of the stress application.

What time scale is expected for gel deformation during extrusion through fractures? In Ref. 1, Cr(III)-acetate-HPAM gel injection fluxes were between 0.046 and 11.7 cm/s in fractures with widths of 0.1 cm. Because of the wormholing effect described in Ref. 1, the actual gel velocity may have been 20 times greater—up to 250 cm/s. In the analysis of Fig. 2, we suggested that this gel could deform in a Hookean fashion up to 200% and deform up to 4,300% before breaking. Thus, in a 0.1-cm-wide fracture, an element of gel may stretch between 0.2 and 43 cm before breaking. Perhaps elements of gel propagate through the fracture in jumps between 0.2 and 43 cm. If so, an element of gel propagating with a velocity of 250 cm/s would experience cycles of deformation (i.e., jumps) every 0.001 to 0.1 seconds. This calculation suggests that the frequency of deformation may be in the range from 10 to 1,000 s⁻¹ during this extrusion experiment.

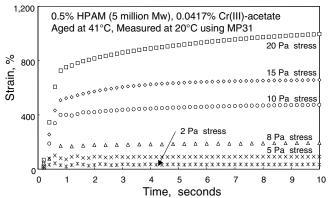


Fig. 6—Strain vs. time.

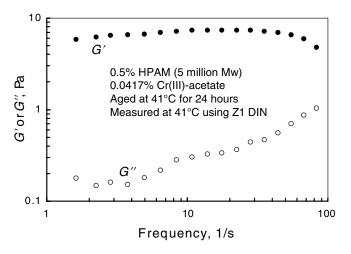


Fig. 7—G' and G'' vs. frequency.

G' and G" vs. Frequency

The above calculation raises the following question: How do G' and G'' vary with the applied frequency of oscillation? **Fig. 7** plots G' and G'' for the Cr(III)-acetate-HPAM gel for frequencies ranging from 1 to $100 \, \mathrm{s^{-1}}$. Instead of the plate-plate geometry (MP31) used in the previous experiments, these measurements were made using a double-gap concentric cylinder (Z1 DIN). This device had a bob length of 11.1 cm, gap widths of 0.05 cm, and average bob radii of 2.3 cm. As with the previous experiments, the gel was aged for 24 hours at 41°C; then the measurements were taken at 41°C.

G' was fairly constant for frequencies from 1 to $100 \, \mathrm{s^{-1}}$. This observation was consistent with those reported by previous researchers using other gels. $^{7.8,11,12}$ In Fig. 7, G'' increased moderately with increased frequency. The behavior for both G' and G'' were qualitatively similar to those for rubber. 16 In contrast, for concentrated, uncrosslinked polymeric liquids, G' and G'' increase significantly with increased frequency, except for a limited region of near-constant moduli at intermediate frequencies. 16 Thus, even though our Cr(III)-acetate-HPAM gel can flow (more specifically, extrude) through fractures, its rheology is much closer to rubber than to that of an uncrosslinked polymer solution.

Effect of Temperature

Most measurements to this point were performed at 20° C, even though the gels were aged at 41° C. Does G' depend on temperature? This question is addressed in **Fig. 8** for our standard Cr(III)-acetate-HPAM gel. Investigated temperatures ranged from 15 to 45° C. The applied strain was 40% during the measurements and the frequency was 1 Hz. In all cases, the gel was prepared in the same way and aged for 24 hours at 41° C before measurement at the specified temperature.

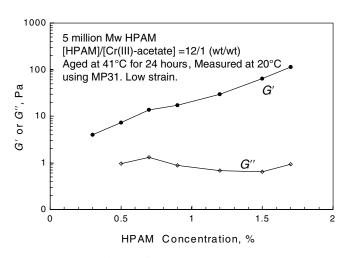


Fig. 9—G' and G'' vs. polymer concentration.

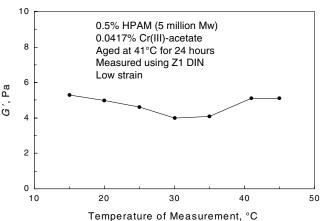


Fig. 8—G' vs. temperature.

G' was fairly insensitive to temperature, averaging about 5 Pa (Fig. 8). The insensitivity of G' to temperature is characteristic of rubber-like materials. ¹⁷ From Fig. 2, G' was expected to be about 10 Pa rather than 5 Pa. The difference may be owing to the different measuring systems that were used. For the experiments shown in Fig. 2, a plate-plate geometry was used (MP31), while the data shown in Fig. 8 were collected using Z1 DIN, a double-gap concentric cylinder. Geometry-dependent measurements are not uncommon among viscometers. ¹⁶

G' and G" vs. Polymer Concentration

The measurements to this point involved a Cr(III)-acetate-HPAM gel that contained 0.5% HPAM and 0.0417% Cr(III)-acetate. How do *G'* and *G''* vary with gel composition? This question is answered in **Fig. 9** for HPAM concentrations ranging from 0.3 to 1.7%. In all cases, the ratio of HPAM concentration to Cr(III)-acetate (weight/weight) was 12 to 1. The brine content was fixed (1% NaCl, 0.1% CaCl₂), the gels were aged at 41°C for 24 hours before testing, and the measurements were made at 20°C using MP31. The applied strain was 40% and the frequency was 1 Hz.

As the polymer concentration in the gel increased from 0.3 to 1.7%, the elastic modulus increased from 4 to 115 Pa. A curve fit to the data in Fig. 9 indicated that G' was roughly proportional to the square of polymer concentration. Reportedly, G' is directly proportional to the density of crosslinks in a gel.⁷⁻⁹

In contrast to G', the viscous modulus (G'') remained near 1 Pa. Thus, as expected, the elastic component became increasingly dominant (over the viscous component) as the polymer concentration increased.

G' vs. Crosslinker Concentration and Type

As mentioned earlier, the polymer-to-crosslinker ratio was fixed for the experiments shown in Fig. 9. Fig. 10 shows the effect of

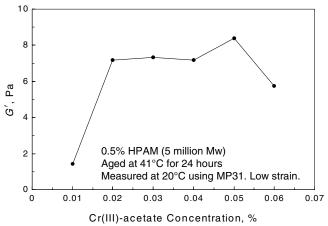


Fig. 10—G' vs. Cr(III)-acetate concentration.

TABLE 1—COMPARISON OF G^{\prime} VALUES FOR VARIOUS GELS	
Gel	<i>G</i> ′, Pa
0.5% HPAM (5 million Mw), 0.0417% Cr(III)-acetate	10
0.5% HPAM (5 million Mw), 0.01% Al(III)-sulfate	2
0.5% HPAM (12 million Mw), 0.0417% Cr(III)-acetate	10
0.2% HPAM (12 million Mw), 0.0167% Cr(III)-acetate	1

crosslinker concentration on G' for a Cr(III)-acetate-HPAM gel that contained 0.5% HPAM. G' exhibited a broad maximum at \sim 7 to 8 Pa for Cr(III)-acetate concentrations between 0.02 and 0.05%. Presumably, over this range of crosslinker concentration, the gel strength and the density of crosslinks were determined by the frequency of polymer chain overlap, which in turn was determined by the polymer concentration rather than by the crosslinker concentration.

We also studied an Al(III)-sulfate-HPAM gel. This gel contained 0.5% Ciba Alcoflood 935 HPAM, 0.01% Al(III)-sulfate, 1% NaCl, and 0.1% CaCl₂. Thus, the composition of the gel was identical to that of the Cr(III)-acetate-HPAM gel, except that a different crosslinker was used. This gel was aged for 24 hours at 41°C. Rheological measurements were made at 20°C and 1 Hz using the MP31 plate-plate system. The elastic modulus was 2 Pa. This value was about one-fifth that for the Cr(III)-acetate-HPAM gel (see **Table 1**). More details of this work can be found in Ref. 18.

Effect of HPAM Molecular Weight

We also examined two Cr(III)-acetate-HPAM gels that were prepared using a polymer (Ciba Percol 338) with roughly twice the molecular weight of Ciba Alcoflood 935. Both polymers had the same degree of hydrolysis. One gel contained 0.5% Percol 338 HPAM and 0.0417% Cr(III)-acetate (the same polymer and crosslinker concentrations in our earlier, standard gel). The second gel contained 0.2% Percol 338 HPAM and 0.0167% Cr(III)-acetate (2.5 times less polymer and crosslinker). Both gels contained 1% NaCl and 0.1% CaCl₂. Both gels were aged for 24 hours at 41°C and the rheological measurements were made at 20°C using MP31.

When the HPAM concentration was 0.5%, G' was 10 Pa for gels prepared from polymers of either molecular weight (**Table 1**). This result was expected. For both gels, the polymer concentration was well above the critical polymer overlap concentration. In that state, the average distance between polymer chain segments determined the gel structure. Since the two gels had the same polymer concentration, the average distance between polymer chain segments and the gel structures was essentially the same.

When the concentration of the high-molecular-weight polymer was 0.2%, G' was about 1 Pa (Table 1). In Ref. 1, we reported that during extrusion of this gel through a 0.1-cm-wide fracture, the pressure gradient was 90~kPa/m. This value was 0.14% of the pressure gradient during extrusion of the gel with 0.5% of the lower-molecular-weight HPAM (our standard Cr(III)-acetate-HPAM gel). Thus, in comparing the two gels, G' appears to correlate qualitatively with the pressure gradient required for gel extrusion through a fracture. However, we had hoped that the correlation would be more quantitative.

Effect of Gel Aging

In field applications where large volumes of gel were injected, the time required to inject the gel was typically 1 week, but could be up to 1 month in some cases. Do the rheological properties of the gel change with time?

Fig. 11 plots G' vs. HPAM concentration for Cr(III)-acetate-HPAM gels that were aged at 41°C for 1 day, 4 days, and 9 days. (Rheological measurements were made at 40% strain and at 20°C using MP31.) HPAM concentrations in these gels ranged from 0.5 to 1.5%. The ratio of polymer to crosslinker was fixed. As noted in Fig. 9, for a given gel at a given time, G' increased with increased HPAM concentration. G' also increased with increased aging time at 41°C. The increase may have been caused by "curing" or more complete intermolecular crosslinking reactions with increased time.

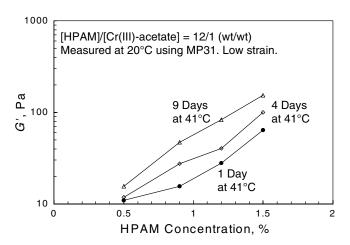


Fig. 11—G' vs. HPAM concentration and storage time.

Unresolved Issues

In this paper, we considered whether rheological measurements can be related to the behavior observed during gel extrusion through fractures. We suggested that an analogy is expected between gel extrusion through fractures and deformation between two plates in a rheometer. However, differences are anticipated as well. We recognize that oscillatory rheological measurements generally do not involve rupture of gel-gel bonds or gel-wall bonds, so they may not correlate with results from extrusion through fractures where bond rupture must occur. Also, gels dehydrate during extrusion through fractures, and the water emanating from the gel is removed by leakoff through the fracture faces. This dehydration process was not taken into account during rheological measurements.

As indicated earlier in this paper, additional work is needed to relate the behavior in rheometers quantitatively to that during extrusion through fractures. In particular, some of the unresolved questions include the following:

- 1. Why is the pressure gradient during gel extrusion through fractures substantially greater than the value expected from rheological measurements?
- 2. Why does the pressure gradient for gel extrusion through fractures vary inversely with the square of fracture width?

Conclusions

- 1. For a 24-hour-old Cr(III)-acetate-HPAM gel, the elastic modulus (G') was fairly constant for strain values up to 200%. The elastic nature of these gels was evident even at strain values over 1,000%. This finding is consistent with the ease with which these gels extrude through fractures.
- 2. As the polymer concentration in the gel increased from 0.3 to 1.7%, the elastic modulus increased from 4 to 115 Pa. In contrast, the viscous modulus (G") remained near 1 Pa. Thus, as expected, the elastic component became increasingly dominant (over the viscous component) as the polymer concentration increased. The temperature and frequency dependencies of the elastic modulus were characteristic of those for rubber-like materials.
- 3. For gels that contained 0.5% HPAM, *G'* showed a broad maximum at ~7 to 8 Pa for Cr(III)-acetate concentrations between 0.02 and 0.05%.
- 4. Shear stress was fairly insensitive to shear rate. When shear rate was increased by a factor of 100,000, shear stress only increased by a factor of 10. This result was consistent with our earlier observations that the pressure gradient required to extrude a gel through a fracture was fairly insensitive to injection velocity.
- 5. A log-log plot of complex viscosity vs. shear rate gave a slope of −0.8. This value was very similar to that for a log-log plot of resistance factor vs. injection velocity that was noted earlier during gel extrusion through fractures.
- For Cr(III)-acetate-HPAM gels, G' increased with increased aging time at 41°C (up to 9 days).

 Considerable additional work is needed to establish a correlation between gel behavior in fractures and in a viscometer.

Nomenclature

C = polymer concentration, %

G =shear modulus, Pa

 $G^* = \text{complex modulus}$, Pa

G' = elastic or storage modulus, Pa

G'' = viscous or loss modulus, Pa

 k_f = fracture permeability, darcies [μ m²]

L = length, ft [m]

dp/dL = pressure gradient, psi/ft [Pa/m]

t = time, s

 w_f = fracture width, in. [m]

Greek Symbols

 δ = phase shift or loss angle, °

 γ = shear strain, %

 $\gamma_o = \text{maximum strain}, \%$

 $\dot{\gamma}$ = shear rate, s⁻¹

 $\dot{\gamma}_o = \text{maximum shear rate, s}^{-1}$

 $\mu' = \text{dynamic viscosity}, \text{Pa} \cdot \text{s}$

 μ'' = elastic component of complex viscosity, Pa·s

 $\mu^* = \text{complex viscosity}, \text{Pa} \cdot \text{s}$

 $\mu_w = \text{water viscosity, cp } [Pa \cdot s]$

 $\tau = \text{stress}, \text{psi [Pa]}$

 τ' = elastic component of stress, psi [Pa]

 τ'' = viscous component of stress, psi [Pa]

 $\tau_o = \text{maximum component of stress, psi [Pa]}$

 $\tau_o' = \text{maximum component of elastic stress, psi [Pa]}$

 τ_o'' = maximum component of viscous stress, psi [Pa]

 τ_s = shear stress, psi [Pa]

 $\tau_{\rm v} = {\rm yield\ stress,\ psi\ [Pa]}$

 $\omega = \text{angular frequency, s}^{-1}$

Acknowledgments

Financial support for this work is gratefully acknowledged from the Natl. Petroleum Technology Office of the U.S. Dept. of Energy, BP plc, Chevron, China Natl. Petroleum Corp., Chinese Petroleum Corp., Halliburton, Marathon, Saga, Schlumberger, Shell, and Texaco.

References

- Seright, R.S.: "Gel Propagation Through Fractures," paper SPE 59316 presented at the 2000 SPE/DOE Symposium on Improved Oil Recovery, Tulsa, Oklahoma, 3–5 April.
- Seright, R.S.: "Gel Placement in Fractured Systems," SPEPF (November 1995) 241; Trans., AIME, 299.
- Seright, R.S.: "Use of Preformed Gels for Conformance Control in Fractured Systems," SPEPF (February 1997) 59.
- Seright, R.S.: "Polymer Gel Dehydration During Extrusion Through Fractures," SPEPF (May 1999) 110.
- Seright, R.S.: "Mechanism for Gel Propagation Through Fractures," paper SPE 55628 presented at the 1999 SPE Rocky Mountain Regional Meeting, Gillette, Wyoming, 15–18 May.
- Seright, R.S.: "Using Chemicals to Optimize Conformance Control in Fractured Reservoirs," Annual Technical Progress Report, U.S. DOE Contract No. DE-AC26-98BC15110, U.S. DOE, Washington, DC (September 2000).

- 7. Prud'homme, R.K. *et al.*: "Rheological Monitoring of the Formation of Polyacrylamide/Cr⁺³ Gels," *SPEJ* (October 1983) 804.
- Prud'homme, R.K. and Uhl, J.T.: "Kinetics of Polymer/Metal-Ion Gelation," paper SPE/DOE 12640 presented at the 1984 AIME SPE/DOE Symposium on Enhanced Oil Recovery, Tulsa, Oklahoma, 15–18 April.
- Pearson, D.S. and Graessley, W.W.: "The Structure of Rubber Networks with Multifunctional Junctions," *Macromolecules* (1978) 11, No. 3, 528.
- Aslam, S., Vossoughi, S., and Willhite, G.P.: "Viscometric Measurement of Chromium(III)-Polyacrylamide Gels by Weissenberg Rheogoniometer," paper SPE 12639 presented at the 1984 AIME SPE/DOE Symposium on Enhanced Oil Recovery, Tulsa, Oklahoma, 15–18 April.
- Thurston, G.B., Ozon, P.M., and Pope, G.A.: "The Viscoelasticity and Gelation of Some Polyacrylamide and Xanthan Gum Solutions," paper available from SPE, Richardson, Texas (1985).
- 12. Kakadjian, S., Rauseo, O., and Mejias, F.: "Dynamic Rheology as a Method to Quantify Gel Strength of Water Shutoff Systems," paper SPE 50751 presented at the 1999 International Symposium on Oilfield Chemistry, Houston, 16–19 February.
- Allain, C. and Salome, L.: "Gelation of Semidilute Polymer Solutions by Ion Complexation: Critical Behavior of the Rheological Properties vs. Cross-Link Concentration," *Macromolecules* (1990) 23, No. 4, 981.
- 14. Broseta, D. et al.: "Rheological Screening of Low-Molecular-Weight Polyacrylamide/Chromium(III) Acetate Water Shutoff Gels," paper SPE 59319 presented at the 2000 SPE/DOE Symposium on Improved Oil Recovery, Tulsa, Oklahoma, 3–5 April.
- Callister, W.D. Jr.: Materials Science and Engineering, An Introduction, fourth edition, John Wiley & Sons Inc., New York City (1997) 108–140.
- Macosko, C.W.: Rheology Principles, Measurements, and Applications, WILEY-VCH, New York City (1994) 108–140, 175–378.
- Aklonis, J.J. and MacKnight, W.W.: Introduction to Polymer Viscoelasticity, second edition, John Wiley and Sons Inc., New York City (1983) 102–138.
- Seright, R.S.: "Using Chemicals to Optimize Conformance Control in Fractured Reservoirs," Annual Technical Progress Report, Contract No. DE-AC26-98BC15110, U.S. DOE, Washington, DC (September 1999).

SI Metric Conversion Factors

 $cp \times 1.0^*$ $E - 03 = Pa \cdot s$ $ft \times 3.048^*$ E - 01 = m $in. \times 2.54^*$ E + 00 = cm $psi \times 6.894757$ E + 00 = kPa

*Conversion factor is exact.

SPEJ

Jin Liu worked at the Scientific Research Institute of Petroleum Exploration and Development of the China Natl. Petroleum Corp. in Beijing from 1992 to 1997. She holds a BS degree in applied chemistry from the Southwest Petroleum Inst., Nanchong, China, and an MS degree in petroleum engineering from New Mexico Tech. Randy Seright is a senior engineer at the New Mexico Petroleum Recovery Research Center in Socorro, New Mexico. e-mail: randy@prrc.nmt.edu. He holds a BS degree in chemical engineering from Montana State U. and a PhD degree in chemical engineering from the U. of Wisconsin. Seright is a member of the SPE Board of Directors, representing the Southwest North America Region for the period 2000–02, and he won a Regional Service Award in 1999.